MODELING MICROBIALLY-MEDIATED CONSUMPTION OF OXYGEN TRAPPED IN VOIDS OF A POTENTIAL REPOSITORY AFTER BACKFILLING AT ÄSPÖ SITE

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ABSTRACT. The presence of molecular oxygen left in the voids of a deep geological repository of high level radioactive waste (HLW) after backfilling could affect the corrosion of canisters and the migration of radionuclides eventually released from a damaged canister. Knowing how O₂ is consumed is therefore important for safety analyses. Available data from laboratory and in situ experiments indicate that microbes play a substantial role to restore redox condition near the HLW repository. The REX in situ experiment was conducted at the Äspö Hard Rock Laboratory by the Swedish Nuclear Waste Management Company to investigate microbial nutrients, organism diversity, microbial activity and O₂ reduction. This paper presents a hydro-bio-geochemical model to evaluate how O₂ is consumed after backfilling of a HLW repository planned according to the Swedish reference concept. The microbial model accounts for dissolved organic carbon (DOC) respiration and methane oxidation. Parameters for these processes were calibrated with measured oxygen in the REX experiment. Computed concentrations of oxygen match measured data in the chamber of the REX experiment. Calibration results indicate that the microbial model can be used to simulate the processes of O₂ reduction trapped in the voids of the bentonite buffer. The role of microbes in the consumption of O₂ is evaluated for several cases corresponding to various hypotheses. Numerical results show that microbial processes are relevant for O₂ consumption in the repository. The time needed to consume the O₂ trapped in the buffer decreases from over 50 for only geochemical processes to a few months when the catalytic effect of microbes in DOC respiration and methane oxidation is taken into account.

RESUMEN. El oxígeno molecular disuelto en los poros del material de relleno y sellado de un almacenamiento geológico profundo (AGP) de residuos radiactivos después de su clausura podría afectar negativamente en la corrosión de los contenedores y en la migración de los radionucleidos que se pueden liberar tras el colapso del contenedor. Para la evaluación de la seguridad de un AGP es importante saber cómo se consume el O₂. Los datos disponibles procedentes tanto de ensayos de laboratorio como ensayos in situ en

laboratorios subterráneos indican que los microorganismos desempeñan un papel relevante en el restablecimiento de las condiciones redox en el entorno de un AGP. El experimento in situ REX fue realizado en el laboratorio subterráneo de Äspö (Suecia) por SKB (compañía sueca para la gestión de residuos radiactivos) para estudiar los nutrientes microbiológicos, la diversidad de microorganismos y su actividad. Este trabajo presenta un modelo acoplado hidro-bio-geoquímico para evaluar la reducción del O2 disuelto presente en la barrera de bentonita de un AGP de las características contempladas por SKB. El modelo microbiológico tiene en cuenta la respiración del carbono orgánico disuelto (DOC) y la oxidación del metano. Los parámetros para estos procesos han sido calibrados con los valores de oxígeno medidos en el experimento REX. Los valores calculados de la concentración de oxígeno reproducen los datos medidos en la cámara del citado experimento. Los resultados de la calibración indican que el modelo microbiológico puede ser utilizado para simular los procesos de reducción del O2. El papel de los microorganismos en la reducción del O2 se analiza con varias hipótesis. Los resultados numéricos muestran que los procesos microbiológicos son relevantes para la desaparición del O2 en el AGP. La reducción del oxígeno mediante procesos exclusivamente químicos requiere casi 50 años para agotar el O2 atrapado en la bentonita. Este tiempo se reduce a unos pocos meses cuando se considera además de los procesos químicos el papel catalizador de los microorganismos de los procesos de respiración del DOC y la oxidación del metano.

1. Introduction

Underground facilities are being operated by several countries around the world for performing research and providing demonstration of the safety of deep radioactive waste repositories. The Äspö Hard Rock Laboratory is one of such facilities launched and operated by the Swedish Nuclear Waste Management Company where various in situ experiments have been carried out in fractured granites.

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One of the main tasks of those experiments is to evaluate the stability of redox conditions in the engineered barriers and the surrounding rock. Redox conditions in deep hard rock environments are usually stable with redox potentials between -100 and -400 mV (Haveman et al. 1998). When the repository is constructed, oxygen could be introduced and the redox conditions could be affected. After the tunnels have been sealed, oxygen will still remain trapped in backfilling and buffer materials. Therefore, evaluating consumption of O_2 is very important for the performance assessment of a HLW repository.

Several researchers reported that microbes could catalyze redox reactions in the repository environment and take a significant role in the stability of redox condition in the area adjacent to and within nuclear waste canisters (Pedersen 1995, 1999, 2000a, 2000b, Jolley et al. 2003). Available data from *REX* in situ experiment at Äspö site conducted by SKB confirm that microbes play a substantial role in O₂ consumption. This experiment studied O₂ depletion processes by imposing a controlled oxidizing perturbation in a deep rock environment at the Äspö site. Oxygen was injected into a fracture zone and water samples were collected for microbiological analyses. The REX niche is located 380 m below ground surface. The experiment was performed in a closed recirculating system placed in a borehole.

The circulation loop had a total volume of about 1 L, and before each O_2 pulse it was filled with fresh O_2 -free groundwater from an adjacent borehole. O_2 injection pulses started by replacing part of the volume by groundwater samples that had been previously saturated with either air or $O_{2(g)}$ (Puigdomenech et al. 2001).

The main objective of this paper is to present a hydrobiogeochemical model to evaluate the role of microbes in the consumption of O₂ trapped in the voids after backfilling a potential repository. BIOCORE^{2D} is used to solve the coupled model.

BIOCORE^{2D} is a general purpose code, presented by Zhang (2001) and improved by Samper et al. (2005a). BIOCORE^{2D} incorporates groundwater flow, thermal and multicomponet solute transport in variably saturated porous media with a complete suite of abiotic, such as aqueous complexation, adsorption, ion-exchange, redox, precipitation-dissolution, acid-base reactions, and microbial growth transformation processes accounting for metabolic competition, decay, metabiosis and endogeneous respiration and the resistance of the biofilm to the substrates.

BIOCORE^{2D} has been verified with some other codes, such as BIOCLOG3D (Engesgaard, 2000) and FEREACT (Tebes et al., 1998). BIOCORE^{2D} has been applied to several real cases, such as the biotransformation of Fe(III) mineral (goethite) to Fe(II) mineral (pyrite) in the near field of Boom clay (Zhang, 2001) and the interpretation of the increase in concentrations of bicarbonate and sulfate measured at the in situ Redox Experiment (Samper et al. 2004, Molinero et al. 2004).

2. Microbial models

The in situ REX experiment shows that different microbial groups could theoretically contribute to the reduction of oxygen at the Äspö site and two microbial processes control oxygen consumption. One is DOC respiration and the other is methane oxidation (Samper et al. 2005a).

2.1. DOC Respiration

Dissolved Organic Carbon (DOC) is a complex mixture of substances derived from biotic and abiotic reactions. It is both consumed and produced by microorganisms. One of the substances, glucose, is an easily respirable substrate, but it is normally not found in groundwaters. Acetate is a key intermediate product in anaerobic metabolism of organic matter both in marine and groundwater environments, being the main product of anaerobic DOC degradation. Formate is also an important intermediate compound in anaerobic reactions. Formate may be present as a transit molecule in methabolic pathways. Both processes have been lumped into a single process "DOC-respiration" in this study. Microbial aerobic respiration of DOC is a very efficient process for oxygen consumption in groundwaters. This process has been extensively studied at the REX project of the Äspö HRL (Samper et al. 2005). Aerobic heterotrophic bacteria are expected to play a relevant role in the postclosure stage of a repository. DOC respiration is simplified to proceed according to:

$$CH_2O + O_2 \xrightarrow{\text{heterotrophs}} HCO_3^- + H^+ + Biomass$$

Microorganisms performing the catalysis of this process are aerobic heterotrophs, probably of the bacterial group pseudomonas. The growth rate of heterotrophic microbes, r_{arowth}^{het} , is assumed to follow a dual Monod kinetics:

$$r_{growth}^{het} = \mu_{het} C_{het} \frac{C_{DOC}}{(K_{DOC} + C_{DOC})} \frac{C_{O_2}}{(K_{O_2} + C_{O_2})}$$
 (1)

where C_{het} is the concentration of aerobic heterotrophs, μ_{het} is the specific growth rate, subindexes DOC and O_2 refer to dissolved organic matter (substrate) and oxygen (electron acceptor), respectively and, K denotes half-saturation constants.

The rate of dissolve organic matter consumption, r_{DOC} , is related to the rate of microbial growth through:

$$r_{DOC} = \frac{1}{Y_{DOC}} r_{growth}^{het} \tag{2}$$

The consumption rate of electron acceptor, r_{O_2} , is related to the rate of microbial growth through:

$$r_{O_2} = \frac{f_{O_2}}{Y_{DOC}} r_{growth}^{het} \tag{3}$$

where Y_{DOC} is the yield coefficient, f_{O2} is the proportionality coefficient between consumed substrate and electron acceptor, which is equal to 1.

Available values of DOC respiration kinetic parameters have been reported by several researchers (Qu and Bhattacharya, 1996, Kotelnikova & Pedersen 1999). Vogelaar et al. (2003) also reported kinetic parameters describing the growth and decay of mesophilic (30 °C) aerobic biomass, a kind of bacteria involved in the degradation of DOC. The parameters were determined in continuous and batch experiments from measured oxygen uptake rates. The intrinsic maximum growth rate was 0.48 \pm 0.11 h⁻¹ while biomass decay rate was 0.004 h⁻¹. Biomass yield coefficient takes a value of 0.5 g biomass per gram of acetate.

2.2. Methane oxidation

The REX project revealed that methane oxidyzers are very common in the Äspö HRL tunnel (Kotelnikova & Pedersen, 1999). CH₄ and H₂ have been detected in all investigated boreholes in Äspö with concentrations which exceed the half-saturation constants of competent microorganisms able to oxidize those substrates. This indicates that concentrations of these compounds are large enough to support significant microbial growth. Measured concentrations of dissolved methane in Äspö groundwaters range from 0.9 up to 980 µM. Active methanotrophic bacteria have been found in Äspö groundwaters. In fact a new species, Methylomonas Scandinavica, was isolated from Aspö groundwaters and characterized for the first time (Kalyuznaya et al., 1999). Physiological characterization of Methylomonas Scandinavica revealed that this species is able to grow in the range of 5-30 °C and pH = 5.0-9.0, with optimal growth at 17 °C and pH =6.8-7.8. It was also found that it corresponds to a halophilic species which is able to grow in a wide range of salinity. This species is clearly adapted to the environmental conditions prevailing at the Åspö site.

Methanotrophic bacteria are relevant microbial species in the consumption of oxygen. In this case, methanotrophs are expected to be one important oxygen consumers in the geosphere.

Microbially-driven methane oxidation is assumed to proceed according to the following reaction:

$$CH_4 + 2O_2 \longrightarrow HCO_3^- + H^+ + H_2O + Biomass$$

which is catalyzed by Methylomonas Scandinavica. The growth rate of methanotrophic bacteria, r_{growth}^{met} , is governed by dual Monod kinetics,

$$r_{growth}^{met} = \mu_{met} C_{met} \frac{C_{CH_4}}{K_{CH_4} + C_{CH_4}} \frac{C_{O_2}}{K_{O_2} + C_{O_2}}$$
(4)

where C_{met} is the concentration of aerobic methanotrophs, μ_{met} is the maximum growth rate, and subindexes CH_4 and O_2 refer to dissolved methane (substrate) and oxygen (electron acceptor), respectively. The rate of substrate consumption (methane) is related to microbial growth rate through

$$r_{CH_4}^{met} = \frac{1}{Y_{CH_4}} r_{growth}^{met} \tag{5}$$

Similarly, the rate of electron acceptor, $\mathit{r_{O_2}^{met}}$, is related to microbial growth rate through

$$r_{O_2}^{met} = \frac{f_{O_2}}{Y_{CH_1}} r_{growth}^{met} \tag{6}$$

where Y_{CH4} is yield coefficient, and f_{O2} is proportionality coefficient between consumed substrate and consumed electron acceptor.

Pedersen (1992) reported the following values for maximum growth rate, decay rate and yield coefficient of methane oxidizer: $12.9 d^{-1}$, $0.96 d^{-1}$ and 0.57 gbiomass/gCH₄, respectively. A detailed survey of microbial kinetic parameters is presented by Samper et al. (2005a).

2.3. Model calibration

Both microbial processes take O₂ as an electron acceptor and compete to consume O2. The consumption rate of O2 depends on the values of microbial kinetic parameters in 1 to 6. Therefore, it is crucial to chose proper values of kinetic parameters to simulate the consumption of oxygen trapped in voids of the repository.

Using the reported values of microbial kinetic parameters, the microbial model was calibrated by trial and error to fit the data of oxygen measured in the REX in situ experiment (Samper et al., 2005a).

The calibrated kinetic parameters are listed in Table 1. Fig. 1 shows the computed and measured time evolutions of oxygen concentration. It can be seen that computed concentrations of oxygen match well measured data in the *REX* Experiment.

Table 1. Calibrated kinetic parameters for two microbial processes at the Äs

	Parameter	Calibrated Value
Methane oxidation	Maximum growth rate Yield coefficient	0.215 d ⁻¹ 0.41 gB / gCH ₂
	Half-saturation methane Half-saturation oxygen	32.5 μM 1.5 μM
DOC Respiration	Maximum growth rate Decay rate Yield coefficient Half saturation DOC	0.48 h 0.04 h 0.04 h 0.5 gBiomass / gDOC
10.00 9.00 (7.00 7.00		REX EXPERIMENT Time evolution at the REX chamber RUNE13 Pulse 28/02/1999

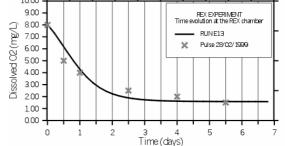


Fig. 1. Computed (line) and measured dissolved oxygen concentration

3. Evaluating consumption of O_2 left in the bentonite after the backfilling

3.1. Hydrobiogeochemical model

The consumption of O₂ trapped in the voids of a potential repository is evaluated with a multicomponent reactive model which accounts for 18 primary species, more than 60 aqueous complexes, 7 minerals (two of them are kinetically controlled) and 2 microbes (see Table 2) (Samper et al. 2005b). The model domain includes a 2D axisymmetric domain (Fig. 2), which consists of two material zones: granite and bentonite. Solute transport takes place only by diffusion.

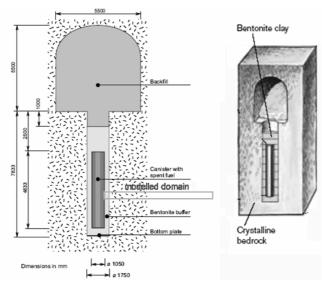


Fig. 2. Scheme of model domain for the O_2 consumption in the bentonite buffer.

The inner boundary is assumed impervious while at the outer boundary the concentration is prescribed. The model considers the Äspö granite and the bentonite buffer made of MX-80 bentonite. The bentonite buffer is assumed to be water saturated. Chemical compositions of granite and bentonite porewater as well boundary water are listed in Table 3. Chemical composition of granitic water was selected from water samples collected on February 6th 1998 at borehole KA2861A (Samper et al., 2005a and b). The composition of initial water in bentonite considered in the numerical model of the LOT experiment by Arcos et al. (2003) was adopted in the current model except for oxygen. The initial concentration of $O_{2(aq)}$ in the bentonite has been assumed to be equilibrated with O2(gas) in the atmosphere before the repository is closed. Granitic water is initially reducing and assumed to be rich in organic matter. After the backfilling, O2 in the bentonite will simultaneously react with iron minerals presenting in bentonite and diffuses into granitic porewater. In the granite, O2 will be available for methylomonas and heterotrophs, as well as for abiotic chemical processes. Initially, neither biomass nor organic matters (DOC and methane) occur in bentonite. The initial concentrations of organic matter and biomass in granite are derived from the *REX* experiment (Samper et al. 2005b).

Pyrite and chlorite are important inorganic reductants. Their dissolution is kinetically controlled dissolution in the near field of HLW repository. Brandt et al. (2003) reported a value of steady-state dissolution rate of chlorite (at 25°C and pH=5) of 10⁻¹³ mol/m²s. Similar results were obtained by Gustafsson and Puigdomenech (2003) for Swedish chlorites. These authors reported dissolution rates within the range of 4x10⁻¹³ mol/m²s for pH = 7, and 3x10⁻¹² mol/m²s for pH = 12. According to these values, a constant reaction rate of 10⁻¹² mol/m²s was adopted for chlorite. Kinetics of pyrite oxidation has been studied extensively (Evangelou et al., 1998; Williamson and Rimstidt, 1994). According to these authors, the kinetic oxidation of pyrite has been simulated as a function of pH and dissolved oxygen concentration, according to:

$$r_m = \kappa_e C_{O_2}^{0.5} C_{H^+}^{-0.11} \tag{7}$$

where κ_e is the effective kinetic rate constant which is equal to $6.5 \cdot 10^{-9} \, \text{mol/m}^2/\text{s}$.

Table 2. Geochemical and microbial components and processes considered in the hydrobiogeochemical model

$ \begin{array}{c} \text{Components} & Br^{\text{-}} \text{Ca}^{+2} \text{Cl}^{\text{-}} \text{Fe}^{+2} \text{H}_2\text{O}, H^{\text{+}} \text{HCO}_3^{\text{-}} \text{K}^{\text{+}} \text{Li}^{\text{+}} \text{Mg}^{+2}, \text{Mn}^{+2}, \\ Na^{\text{+}}, O_{2(aq)}, SiO_{2(aq)}, SO_4^{-2} \text{Sr}^{+2} \text{CH}_4, DOC \\ \hline & Ca(H_3SiO_4)_{2(aq)}, CaCl^{\text{+}}, CaCl_{2(aq)}, CaCO_{3(aq)}, CaH_2SiO_{4(aq)}, \\ CaH_3SiO_4^{\text{+}}, CaHCO_3^{\text{+}}, CaOH^{\text{+}}, CaSO_{4(aq)}, CO_{2(aq)}, CO_3^{-2}, \\ Fe(OH)_{2(aq)}, Fe(OH)_2^{\text{+}}, Fe(OH)_{3(aq)}, Fe(OH)_4^{\text{+}}, Fe^{\text{+}3}, FeCl^{\text{+}}, \\ FeCl_{2(aq)}, FeCl_4^{-2}, FeCO_{3(aq)}, FeCO^3^{\text{+}}, FeHCO_3^{\text{+}}, FeOH^2, \\ FeSO_{4(aq)}, H_{2(aq)}, H_2SiO_4^{\text{-}2}, H_4(H_2SiO_4)_4^{\text{-}4}, H_6(H_2SiO_4)_4^{\text{-}2}, \\ HCl_{(aq)}, HS^{\text{-}}, HSiO_3^{\text{-}}, HSO_4^{\text{-}}, KBr_{(aq)}, KCl_{(aq)}, KHSO_{4(aq)}, \\ KOH_{(aq)}, KSO_4^{\text{-}}, LiCl_{(aq)}, LiOH_{(aq)}, LiSO_4^{\text{-}}, MgH_3SiO_4^{\text{+}}, MgHCO_3^{\text{-}}, \\ MgCl^{\text{+}}, MgCO_{3(aq)}, MgH_2SiO_{4(aq)}, MgH_3SiO_4^{\text{+}}, MgHCO_3^{\text{+}}, \\ MgSO_{4(aq)}, Mn(OH)_{2(aq)}, Mn_2(OH)_3^{\text{+}}, Mn_2OH^{\text{+}3}, MnCl^{\text{+}}, \\ MnCl^3^{\text{-}}, MnCO_{3(aq)}, MnHCO^3^{\text{+}}, MnO_4^{\text{+}}, MnOH^{\text{+}}, MnSO_{4(aq)}, \\ NaBr_{(aq)}, NaCl_{(aq)}, NaCO_3^{\text{-}}, NaHCO_{3(aq)}, NaHSiO_{3(aq)}, \\ NaOH_{(aq)}, NaSO^4^{\text{-}}, OH^{\text{-}}, SrCl^{\text{+}}, SrCO_{3(aq)}, SrOH^{\text{+}}, srSO_{4(aq)}, \\ Calcite, Siderite, Gypsum, Fe(OH)_3, Quartz, Chlorite, \\ Pyrite \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\$		j g
$ \begin{array}{c} Ca(H_3SiO_4)_{2(aq)}, \; CaCl^{\dagger}, \; CaCl_{2(aq)}, \; CaCO_{3(aq)}, \; CaH_2SiO_{4(aq)}, \\ CaH_3SiO_4^{\dagger}, \; CaHCO_3^{\dagger}, \; CaOH^{\dagger}, \; CaSO_{4(aq)}, \; CO_{2(aq)}, \; CO_3^{2}, \\ Fe(OH)_{2(aq)}, \; Fe(OH)_2^{}, \; Fe(OH)_{3(aq)}, \; Fe(OH)_4^{4}, \; Fe^{3}, \; FeCl^{4}, \\ FeCl_{2(aq)}, \; FeCl_4^{2}, \; FeCO_{3(aq)}, \; FeCO^3^{4}, \; FeHCO_3^{4}, \; FeOH^{+2}, \\ FeSO_{4(aq)}, \; H_{2(aq)}, \; H_2SiO_4^{2}, \; H_4(H_2SiO_4)_4^{4}, \; H_6(H_2SiO_4)^{4}, \\ HCl_{(aq)}, \; HS^{}, \; HSiO_3^{3}, \; HSO_4^{3}, \; KBr_{aq)}, \; KCl_{(aq)}, \; KHSO_{4(aq)}, \\ KOH_{(aq)}, \; KSO_4^{4}, \; LiCl_{(aq)}, \; LiOH_{(aq)}, LiSO_4^{4}, \; Mg(H_3SiO_4)_{2(aq)}, \\ MgCl^{\dagger}, \; MgCO_{3(aq)}, \; MgH_2SiO_{4(aq)}, \; MgH_3SiO_4^{4}, \; MgHCO_3^{4}, \\ MgSO_{4(aq)}, \; Mn(OH)_{2(aq)}, \; Mn_2(OH)_3^{4}, \; Mn_2OH^{\dagger}_3, MnCl^{4}, \\ MnCl^3^{3}, \; MnCO_{3(aq)}, \; MnHCO^3^{4}, \; MnO4^{4}, \; MnOH^{\dagger}_1, \; MnSO_{4(aq)}, \\ NaBr_{(aq)}, \; NaCl_{(aq)}, \; NaCO_3^{3}, \; NaHCO_{3(aq)}, \; NaHSiO_{3(aq)}, \\ NaOH_{(aq)}, \; NaSO^4^{4}, \; OH^{4}, \; SrCO_{3(aq)}, \; SrOH^{\dagger}, \; SrSO_{4(aq)}, \\ Calcite, \; Siderite, \; Gypsum, \; Fe(OH)_3, \; Quartz, \; Chlorite, \\ Pyrite \\ \end{array}$	Components	Br', Ca ⁺² , Cl', Fe ⁺² , H ₂ O, H ⁺ , HCO ₃ ⁻ , K ⁺ , Li ⁺ , Mg ⁺² , Mn ⁺² , Na ⁺ , O _{2(aq)} , SiO _{2(aq)} , SO ₄ ⁻² , Sr ⁺² , CH ₄ , DOC
Pyrite		$\begin{array}{llll} Ca(H_3SiO_4)_{2(aq)}, & CaCI^+, & CaCI_{2(aq)}, & CaCO_{3(aq)}, & CaH_2SiO_{4(aq)}, \\ CaH_3SiO_4^+, & CaHCO_3^+, & CaOH^+, & CaSO_{4(aq)}, & CO_{2(aq)}, & CO_3^{-2}, \\ Fe(OH)_{2(aq)}, & Fe(OH)_2^+, & Fe(OH)_{3(aq)}, & Fe(OH)_4^+, & Fe^{-3}, & FeCI^+, \\ FeCI_{2(aq)}, & FeCI_4^{-2}, & FeCO_{3(aq)}, & FeCO_3^{-3}, & FeHCO_3^+, & FeOH^{+2}, \\ FeSO_{4(aq)}, & H_{2(aq)}, & H_{2SiO_4}^{-2}, & H_{4}(H_2SiO_4)_4^{-4}, & H_{6}(H_2SiO_4)_4^{-2}, \\ HCI_{(aq)}, & HS^-, & HSiO_3^-, & HSO_4^-, & KBr_{(aq)}, & KCI_{(aq)}, & KHSO_{4(aq)}, \\ KOH_{(aq)}, & KSO_4^-, & LiCI_{(aq)}, & LiCH_{(aq)}, & LiSO_4^-, & Mg(H_3SiO_4)_{2(aq)}, \\ MgCI^+, & MgCO_{3(aq)}, & MgH_2SiO_{4(aq)}, & MgH_3SiO_4^+, & MgHCO_3^+, \\ MgSO_{4(aq)}, & Mn(OH)_{2(aq)}, & Mn_2(OH)_3^+, & Mn_2OH^{+3}, MnCI^-, \\ MnCI^3, & MnCO_{3(aq)}, & MnHCO_3^+, & MnO_4^-, & MnOH^+, & MnSO_{4(aq)}, \\ NaBr_{(aq)}, & NaCI_{(aq)}, & NaCO_3^-, & NaHCO_{3(aq)}, & NaHSiO_{3(aq)}, \\ NaOH_{(aq)}, & NaSO_4^+, & OH^-, SrCI_1^+, & SrCO_{3(aq)}, SrOH^+, SrSO_{4(aq)}, \\ \end{array}$
Microbes Methylomonas, Heterotrophs	Minerals	The state of the s
	Microbes	Methylomonas, Heterotrophs

3.2. Results

Six cases have been analyzed numerically in order to evaluate the effects of abiotic or biotic processes in the consumption of O_2 trapped in the bentonite.

Case 1 is designed to simulate the evolution of O_2 in the bentonite considering only diffusion into the granite. Case 2 is based on case 1, but accounts for kinetically-controlled dissolution of chlorite in granite. One of the products of the dissolution of chlorite, Fe(II), is oxidized by O₂ in bentonite. The objective of this case is to evaluate the role of the dissolution of chlorite. Based on Case 2, Case 3 also accounts for kinetically-controlled dissolution of pyrite both in bentonite and granite. Case 4, which is based on Case 3, takes into account the two microbial processes which take place only in the granite. It should be noticed that the concentration of CH₄ is the same in both bentonite and granite in Case 4. Compared with Case 4, Case 5 assumes that there is no organic matter in the bentonite. It is worth noting that Cases 4 and 5 assume that no microbial processes in bentonite. In Case 6 which is similar to Case 4, it is assumed that the two microbial processes can take place in the bentonite with a concentration of organic matter equal to that of granite. This case assumes the unlikely hypothesis that microbes can survive in fully saturated compacted bentonite.

Table 3. Concentrations (M) of initial and boundary waters

Species	Initial waters		Boundary water
1	bentonite	Granite	Doundary water
*Br ⁻		1.16×10 ⁻³	1.16×10 ⁻³
Ca ⁺²	1.85×10^{-2}	1.24×10^{-1}	1.24×10^{-1}
Cl ⁻	1.26×10 ⁻¹	3.69×10^{-1}	3.69×10^{-1}
Fe^{+2}	9.67×10^{-12}	9.67×10^{-6}	9.67×10 ⁻⁶
pН	8.4	7.2	7.2
HCO ₃ -	1.70×10^{-4}	4.60×10^{-4}	4.60×10^{-4}
K^{+}	2.00×10^{-4}	6.73×10^{-4}	6.73×10^{-4}
*Li ⁺		4.52×10^{-4}	4.52×10^{-4}
Mg^{+2}	4.43×10^{-3}	1.78×10^{-3}	1.78×10 ⁻³
$^*Mn^{+2}$		7.83×10 ⁻⁶	7.83×10 ⁻⁶
Na ⁺	2.31×10 ⁻¹	1.42×10^{-1}	1.42×10^{-1}
pE	12.3*	-2.2	-2.2
$SiO_{2(aq)}$	2.49×10^{-4}	7.16×10^{-5}	7.16×10 ⁻⁵
SO_4^{-2}	7.63×10 ⁻²	6.56×10^{-3}	6.56×10^{-3}
Sr^{+2}		7.92×10^{-4}	7.92×10^{-4}
*DOC	$2. \times 10^{-10}$	$2.\times10^{-4}$	$2.\times10^{-4}$
*Heterotrophs	4.×10 ⁻⁸	4	4
(mg/L) *CH ₄	1.×10 ⁻¹⁰	1.×10 ⁻⁴	1.×10 ⁻⁴
*Methylomonas	1. ×10 ⁻⁸		1
(mg/L)	1. ×10	1	1

^{*} that component is not included in the numerical model of LOT experiment by Arcos et al., 2003.

Fig. 3 shows the results of the time evolutions of O_2 in the bentonite computed in Cases 1, 2 and 3. One can see that the concentration of O_2 in the bentonite decreases to 1.21×10^{-4} mol/l after about 1000 years in Case 1, 558 years in Case 2 and 52 years in Case 3. Clearly, the consumption of O_2 by chlorite is much smaller than that of pyrite. For the assumed kinetic rate, pyrite will deplete O_2 in 52 years. A sensitive run was performed in which the kinetic rate of pyrite was 10 times smaller than that in Case 3. The time needed to consumption O_2 increases to 225 years.

Fig. 4 shows the comparison of the time evolutions of O_2 in the bentonite computed in Cases 3 and 5. It can be seen that the time to consume O_2 in the bentonite decreases from 50 years in Case 3 to 28.4 years in Case 5 due to microbial processes in the granite. Therefore, microbial reactions play a relevant role on O_2 consumption.

The comparison of the time evolutions of O_2 in the bentonite computed in Cases 4, 5 and 6 is shown in Fig. 5. Cases 4 and 5 differ only on the concentration of CH_4 in bentonite. In Case 5 the concentration of CH_4 is assumed to be 10^{-10} mol/l instead of 10^{-4} mol/l in Case 4. One can see that the time needed to consume O_2 decreases from 28.4 years in Case 5 to 4.2 years in Case 4 and hence the occurrence of organic matter in bentonite can accelerate the rate of O_2 consumption. In comparison with Case 5, Case 6 assumes that the concentrations of DOC and CH_4 are the same in both bentonite and granite and microbial processes can take place in the bentonite. The time needed to consume O_2 in the bentonite in Case 6 decreases

dramatically to 19 days. According to Pedersen (1995), the assumption of Case 6 that microbial processes can proceed in bentonite seems, however, unrealistic.

Table 4 lists a summary of the times needed to consume O₂ for each one of the 6 cases.

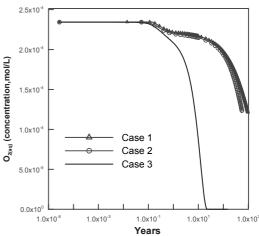


Fig. 3. Comparison of the time evolution of O_2 at a distance of 1dm to the canister in the bentonite computed in Cases 1, 2 and 3.

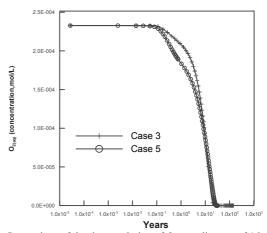


Fig. 4. Comparison of the time evolution of O_2 at a distance of 1dm to the canister in the bentonite computed in Cases 3 and 5.

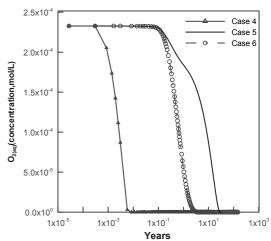


Fig. 5. Comparison of the time evolution of O_2 at a distance of 1dm to the canister in the bentonite computed in Cases 4, 5 and 6.

pE value in the bentonite is different than that in the numerical model of LOT experiment.

Table 4. Time needed to consume O_2 in each one of the 6 cases. Notice that values in parentheses are the concentrations of O_2 (mol/l) in the bentonite at the time indicated in the second column.

Case	Time needed to consume O_2	Threshold O ₂ concentration
1	969 years	(1.21×10 ⁻⁴)
2	558 years	(1.23×10^{-4})
3	51.5 years	(4.15×10^{-30})
4	4.15 years	(1.79×10^{-35})
5	28.4 years	(4.0×10^{-35})
6	19.1 days	(5.35×10^{-30})

4. Conclusions

The results of the 6 cases evaluated allow drawing the following conclusions:

- 1) Dissolution of chlorite in granite is smaller than that of pyrite.
- 2) The effect of pyrite dissolution in the bentonite is important. The time needed to consume O_2 due to the dissolution of pyrite is about 50 years for the parameters and conditions used in the model.
- 3) The effect of microbial processes on O_2 consumption is significant. If microbial reactions can proceed in the bentonite, the time needed to consume O_2 is dramatically decreased to about 2 weeks.
- 4) The presence of dissolved organic matter in bentonite porewater can influence O_2 consumption when microbial reactions can only take place in the granite. The time to consume O_2 decreases from 28.4 without organic matter in the bentonite to 4.2 years when the same concentration of CH_4 is assumed in both granite and bentonite.

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References

- Arcos, D., Bruno, J., Karnland, O. 2003 Geochemical model of the granite-bentonite-groundwater interaction at Äspö HRL (LOT experiment). Applied Clay Science 23, 219-228,
- Brandt, F., Dirk Bosbach, Evelyn Krawczyk-Bärsch, Thuro Arnold, Gert Bernhard. 2003 Chlorite dissolution in the acid pH-range: a combined microscopic and macroscopic approach. *Geochimica et. Cosmochimica Acta*, 67 (8), 1451-1461.
- Engesgaard P. 2000 Model for biological clogging in 3D, Brief user's manual and guide, Department of Hydrodynamics and Water Resources, Danish Technology University.
- Evangelou, V. P. 1998 Environmental soil & water chemistry: Principles and Application. *John Wiley & Sons, Inc.*, New York.
- Gustafsson, A.B. and I. Puigdomenech. 2003 The effect of pH on chlorite dissolution rates at 25°C. Materials Research Society. 757.
- Haveman, S.A., Pedersen K. and Routsalainen P. 1998 Geomicrobial investigations of groundwater from Olkiluoto, Hästholmen, Kivetty and Romuvaara, Finland. POSIVA 98-09.

- Jolley, D.M., Ehrhorn, T. F.and J. Horn. 2003 Microbial Impacts to the Near-Field Environment Geochemistry: a model for estimating microbial communities in repository drifts in Yucca Mountain, *Journal of Contaminant Hydrology* 62-63, 535-575.
- Kalyuznaya, M.G. Khmelenina, V.N., Kotelnikova, S., Pedersen, K., Trotsenko, Y.A. 1999 Methylomonas scandinavica: a New Methanotropic Psychrotrophic Bacterium isolated from Deep Igneous Rock Ground Water of Sweden. Systematic and applied microbiology, 22, 565-572, 1999.
- Kotelnikova, S. and Pedersen, K. 1999 The microbe REX Project: Microbial O_2 consumption in the Äspö tunnel. SKB Technical Report. Stockholm.
- Molinero, J., J. Samper, C. Yang and G. Zhang. 2004 Biogeochemical reactive transport model of the Redox zone experiment of the Äspö hard rock laboratory (Sweden). Vol.48 (2), P151-165 Nuclear Technology.
- Pedersen, K. and Ekendahl, S. 1992 Incorporation of CO₂ and introduced organic compounds by bacterial populations in groundwater from the deep crystalline bedrock of the Stripa mine. *J Gen Microbiol* 138, 369-376.
- Pedersen, K. and F. Karlsson. 1995 Investigation of subterranea n microorganisms – Their importance for performance assessment of radioactive waste disposal. SKB Technical Report 95-10.
- Pedersen, K. 1999 Subterranean microorganisms and radioactive waste disposal in Sweden. *Engineering Geology*, 52 163–176.
- Pedersen, K. 2000a. Microbial processes in radioactive waste disposal. SKB Report.
- Pedersen, K. 2000b. Exploration of deep intraterrestrial microbial life: current perspectives. FEMS Microbiology Letters, 185 9-16.
- Puigdomenech, I., Ambrosi, J.P., Eisenlohr, L., Lartigue, J.E., Banwart, S. A., Bateman, K., Milodowski, A. E. and West, J. M. 2001. O₂ depletion in granitic media. The REX project, *Technical Report*, TR-01-05,1-92.
- Qu, M. B. and Bhattacharya, S. K. 1996. Degradation and toxic effects of acrylic acid on anaerobic systems. *Journal of Environmental Engineering*-ASCE, 122 (8) 749-756.
- Samper, J., J. Molinero, C. B. Yang and G. Zhang. 2004. Redox Zone II. Coupled Modeling of Groundwater Flow, Solute Transport, Chemical reactions and Microbial Processes in the Äspö Island. SKB, *Technical Report*, TR-03-14. Stockholm.
- Samper, J., Molinero, J., Yang, C., Bonilla, M. 2005a. HYDROBIOGEO Project: Modelling hydro-bio-geochemistry in Swedish granites. Report 1: State of the art, compilation of microbial data and processes relevant for Swedish granites, code improvements and hydro-biogeochemical model of the REX experiment. *Tech. Report for SKB* (in review).
- Samper. J., Molinero. J., Yang, C., Bonilla, M. 2005b. HYDROBIOGEO Project: Modelling hydro-bio-geochemistry in Swedish granites. Report 2: Hydro-bio-geochemical model for the consumption of oxygen in the bentonite buffer. *Tech. Report for SKB* (in review).
- Tebes-Stevens C., Valocchi A. J., van Briesen J. M., Rittmann B. E. 1998.Multicomponent Transport with Coupled Geochemical and Microbiological Reactions: Model Description and Example Simulations. Jour. Hydro. 209: 8-26.
- Vogelaar, J.C.T., Klapwijk, B., Temmink, H. and van Lier, J.B. 2003. Kinetic comparisons of mesophilic and thermophilic aerobic biomass. *Journal of Industrial Microbiology & Biotechnology*, 30 (2): 81-88.
- Williamson, M. A., Rimstidt J. D. 1994. The kinetics and electrochemical rate- determining step of aqueous pyrite oxidation. Geochimica et Cosmochimica Acta 58, 5443-5454.
- Zhang, G. and Samper, J., 2001 BIO-CORE^{2DC}, a code for nonisothermal hydrobiogeochemical reactive transport. Users Manual V0. *Technical Report*. University of A Coruña, Spain, p244.